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## 2-D Heat Transfer Model of A Horizontal U-Tube

M. S. Islam<sup>1</sup>, A. Fujimoto<sup>2</sup>, A. Saida<sup>2</sup> and T. Fukuhara<sup>2</sup>

<sup>1</sup> Khulna University of Engineering & Technology, Bangladesh

<sup>2</sup> University of Fukui, Japan

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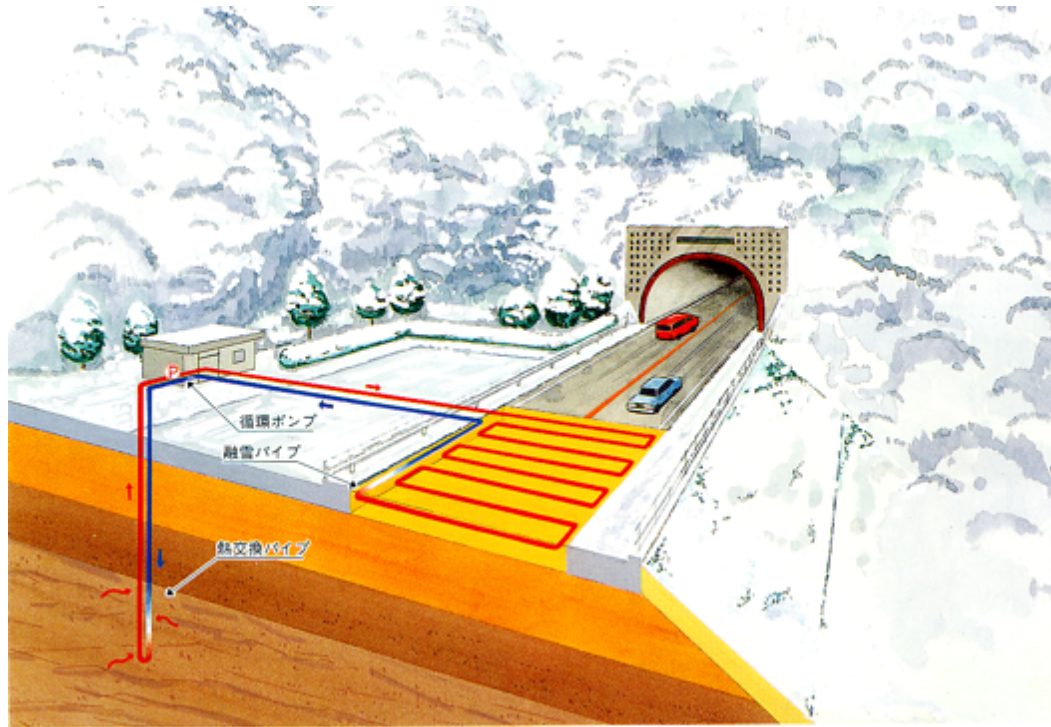
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# Introduction



**A slip accident at specific places such as intersections, bridges, tunnel mouths occurs frequently in winter. because the road surface conditions are remarkably changeable**

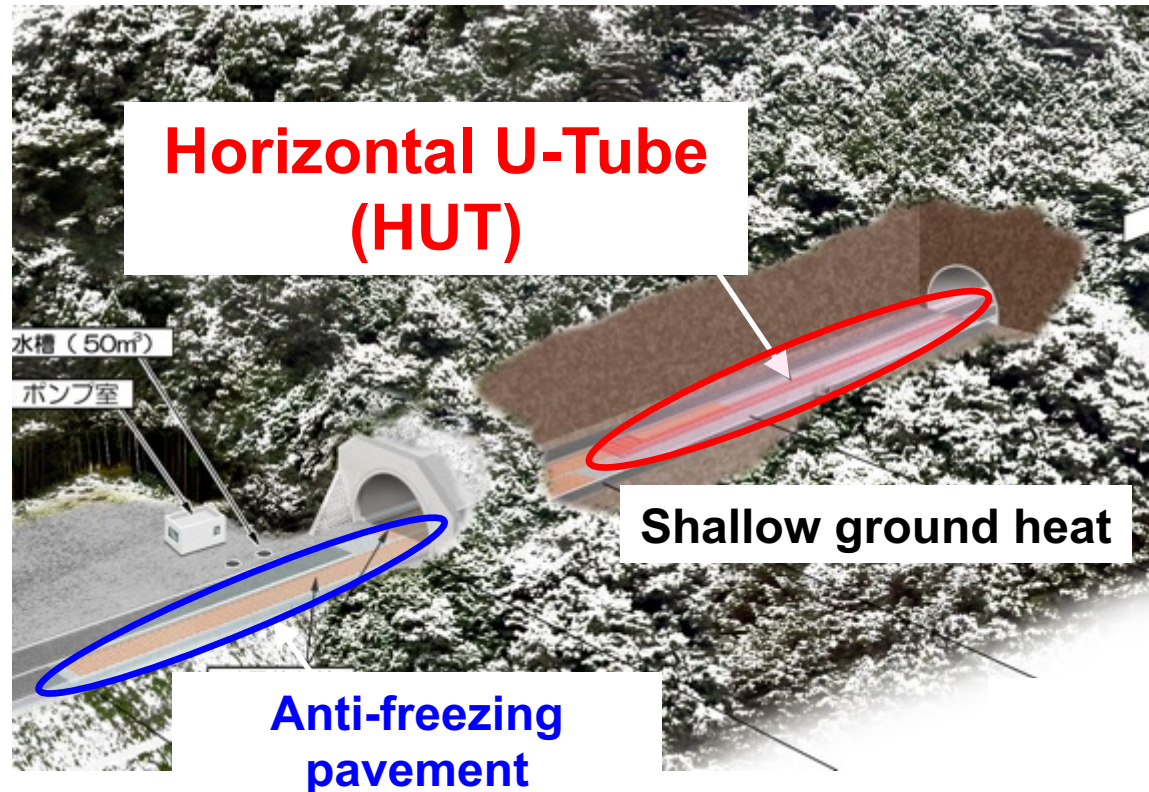
# Introduction



**Road heating system has a significant requirement for reducing winter traffic accidents at the specific places**

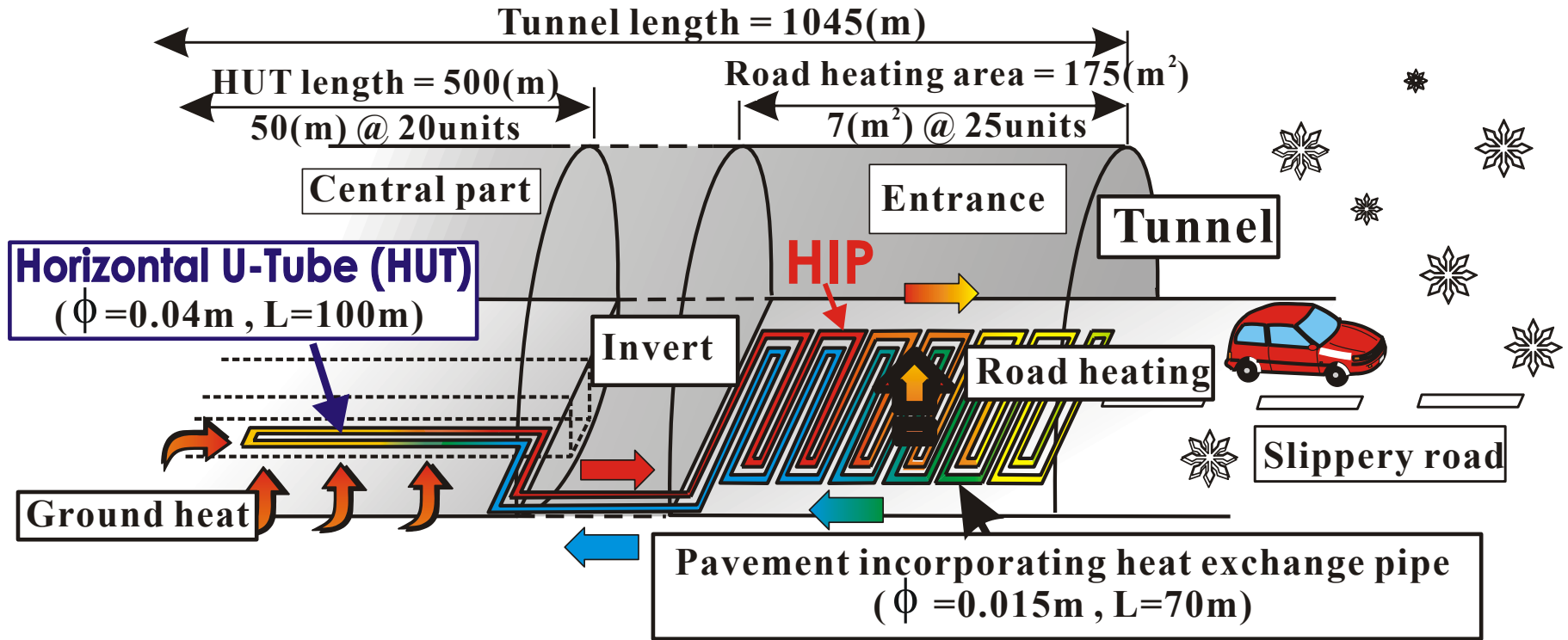


# Introduction



Paying attention to the use of shallow ground heat inside the tunnel, we have been developing Horizontal U-Tube (HUT) road heating system in order to prevent road freezing at tunnel mouth.

# HUT Road Heating System



Since the shallow ground is at a relatively low temperature, the additional HUT length that is also required to heat the road is the length of the HUT and then the length of the HIP.

# Specific Aims

- **To develop heat transfer models of HUT system.**
- **To examine the validity of the proposed models by indoor experiments.**





# Energy Balance Equations

## Ground surrounding HUT

$$(\rho C)_g \frac{\partial T_g}{\partial t} = \frac{\partial}{\partial y} \left( \lambda_g \frac{\partial T_g}{\partial y} \right) + \frac{\partial}{\partial z} \left( \lambda_g \frac{\partial T_g}{\partial z} \right) - \sum_{m=1}^2 E_{(m)} \cdot \eta_g$$

$T_g$  : ground temperature

$(\rho C)_g$  : heat capacity of ground

$\lambda_g$  : thermal conductivity of ground

$E_{(m)}$  : extracted heat flux per unit circumference-surface area of HUT  
[m=1: for going tube, m= 2: for return tube]

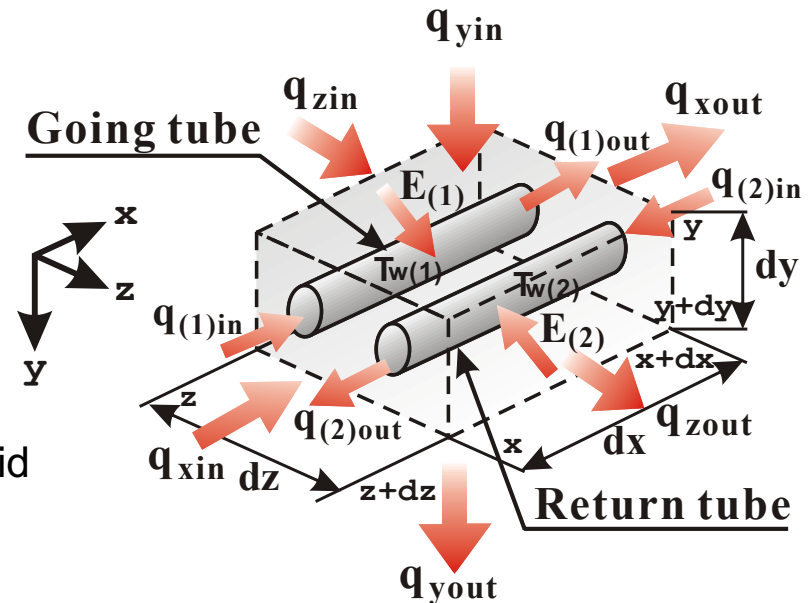
$\eta_g$  : the ratio of the circumference-surface area of HUT to the volume of HUT ground element

## Extracted Heat Flux

$$E_{(m)} = \alpha (T_g - T_{w(m)}) \quad [m=1 \text{ or } 2]$$

$\alpha$  : heat transfer coefficient between HUT fluid and HUT ground.

$T_w$  : HUT fluid temperature



# Energy Balance Equations

## Heat Carrier Fluid of HUT (HUT fluid)

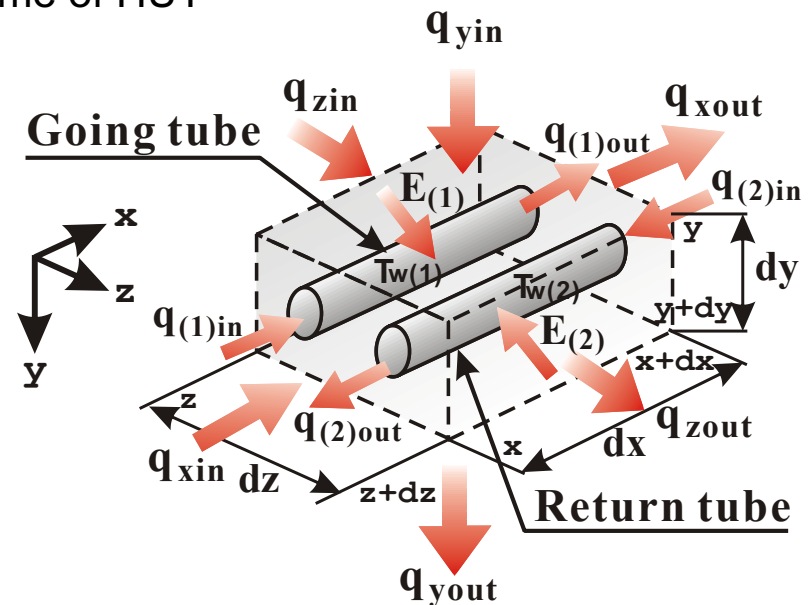
$$(\rho C)_w \frac{\partial T_{w(m)}}{\partial t} = \frac{\partial}{\partial x} \left( \lambda_w \frac{\partial T_{w(m)}}{\partial x} \right) - (\rho C)_w V \frac{\partial T_{w(m)}}{\partial x} + \sum_{m=1}^2 E_{(m)} \cdot \eta_p$$

$(\rho C)_w$  : heat capacity of HUT fluid

$\lambda_w$  : thermal conductivity of HUT fluid

$V$  : velocity of HUT fluid

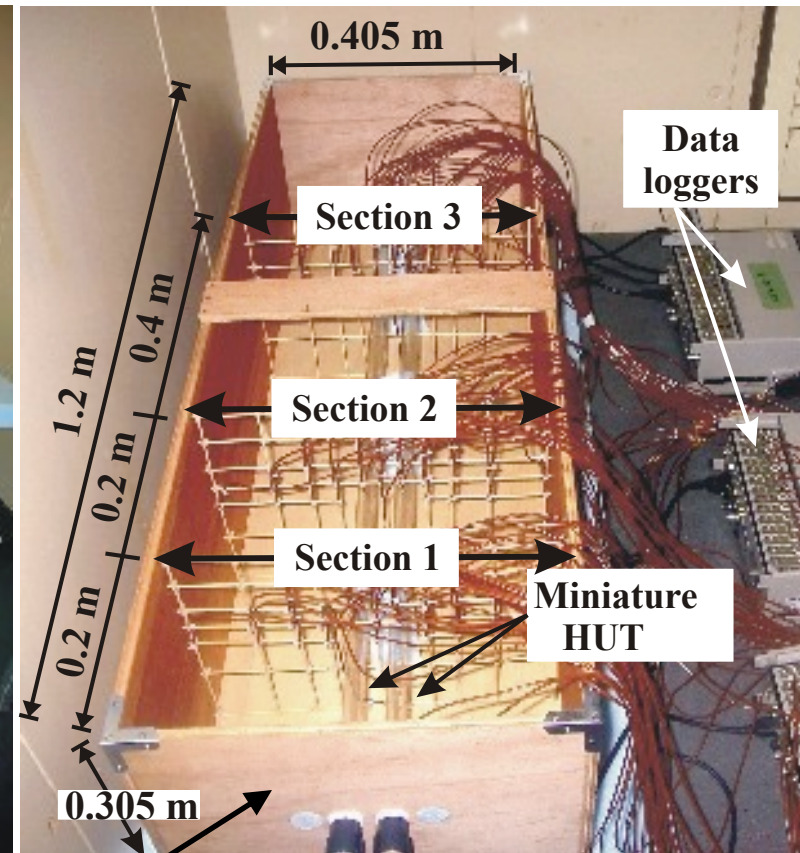
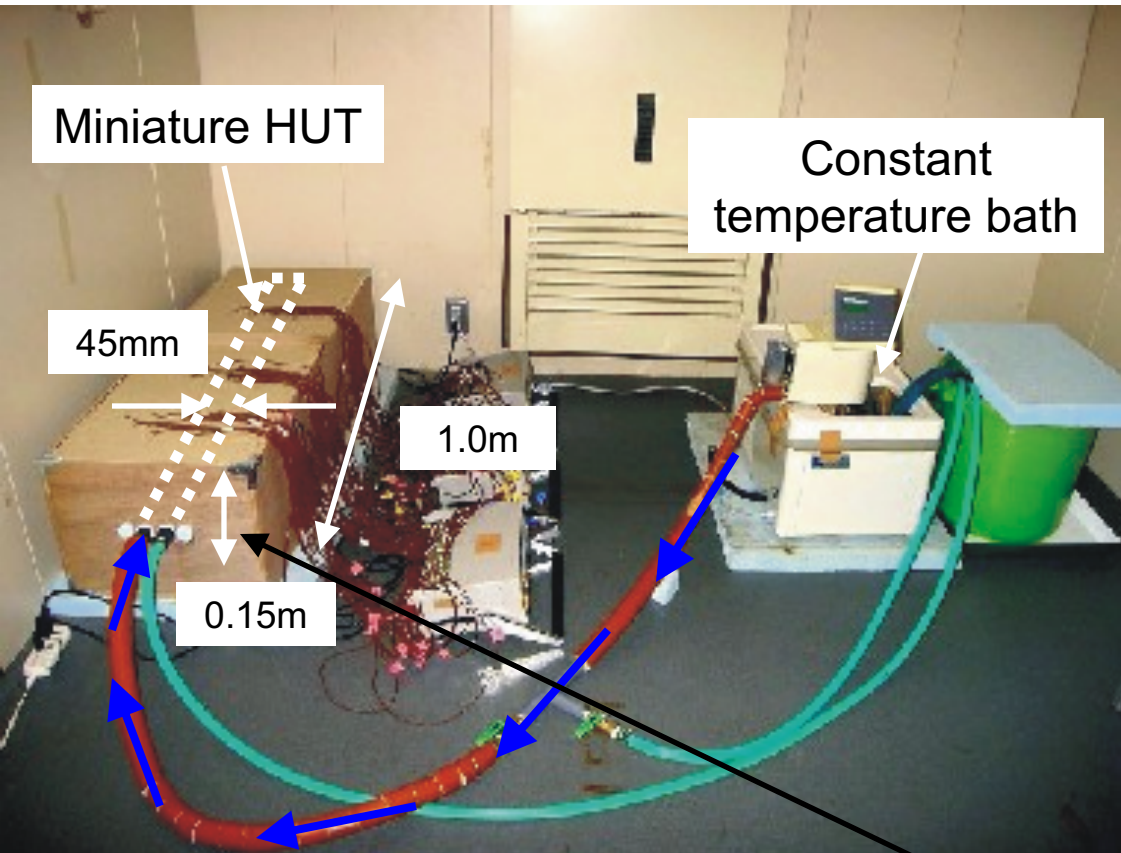
$H_p$  : ratio of circumference-surface area to volume of HUT



2-D Heat Transfer Model of A Horizontal U-Tube

# Indoor Experiments

Air temperature : 25°C



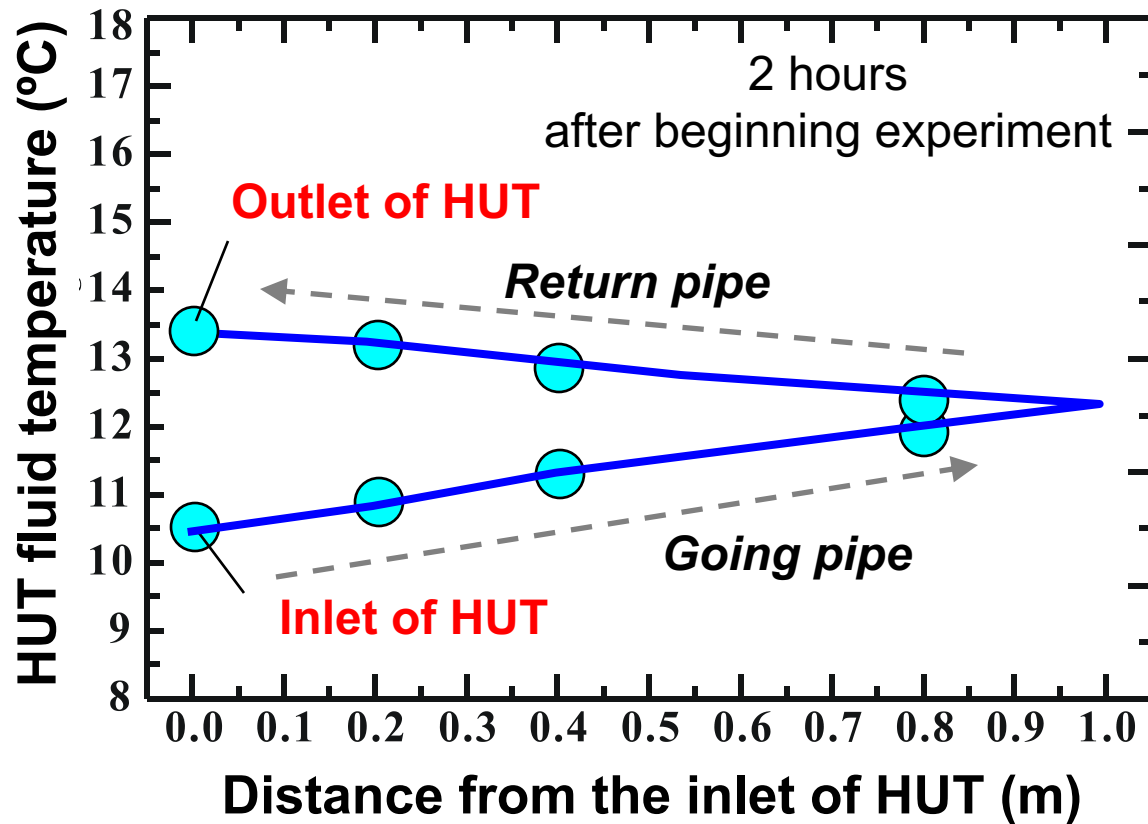
2-D Heat Transfer Model of A Horizontal U-Tube



# Experimental Conditions

Case No.	Room conditions		Flow rate ( $\text{m}^3/\text{sec} \times 10^{-7}$ )
	$T_a$ ( $^{\circ}\text{C}$ )	$\text{RH}_a$ (%)	
1	25	50	7.0
2			12.4
3			20.8
4			25.7
5			47.6

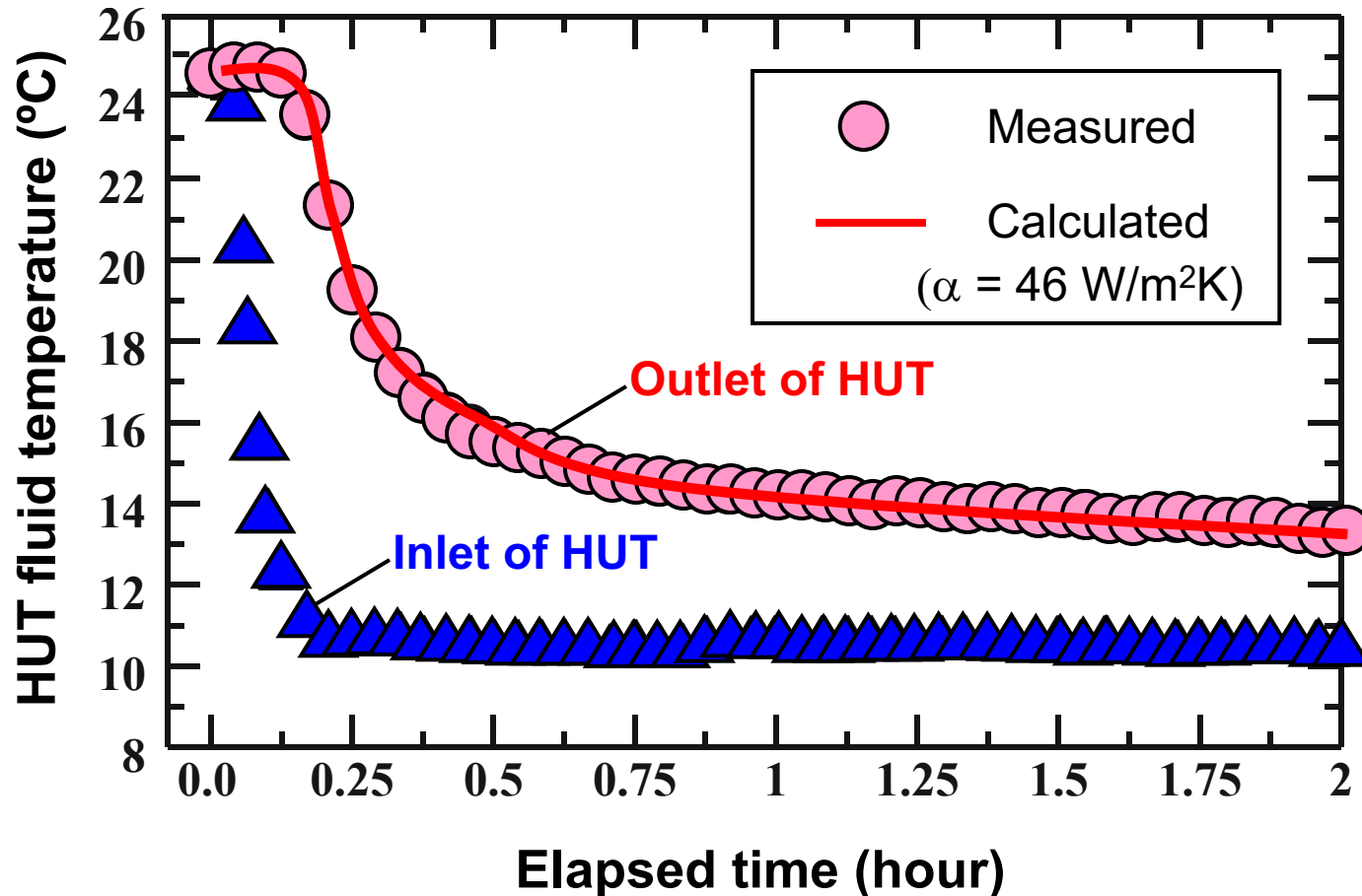
# Longitudinal profile of HUT fluid temperature



Flow rate:  $47.6 \times 10^{-7} \text{ m}^3/\text{sec}$

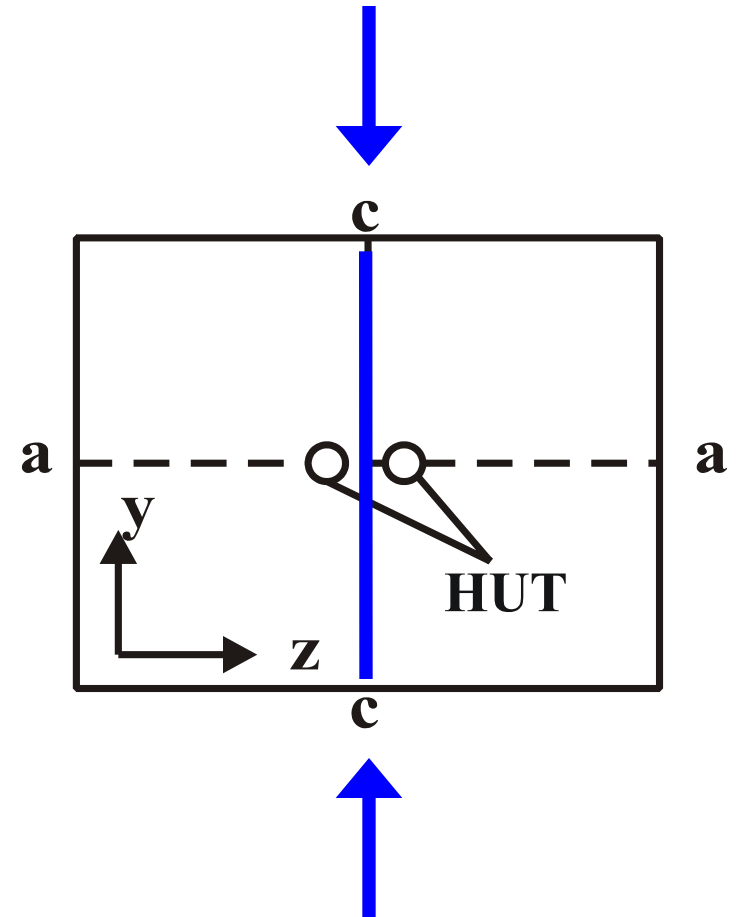
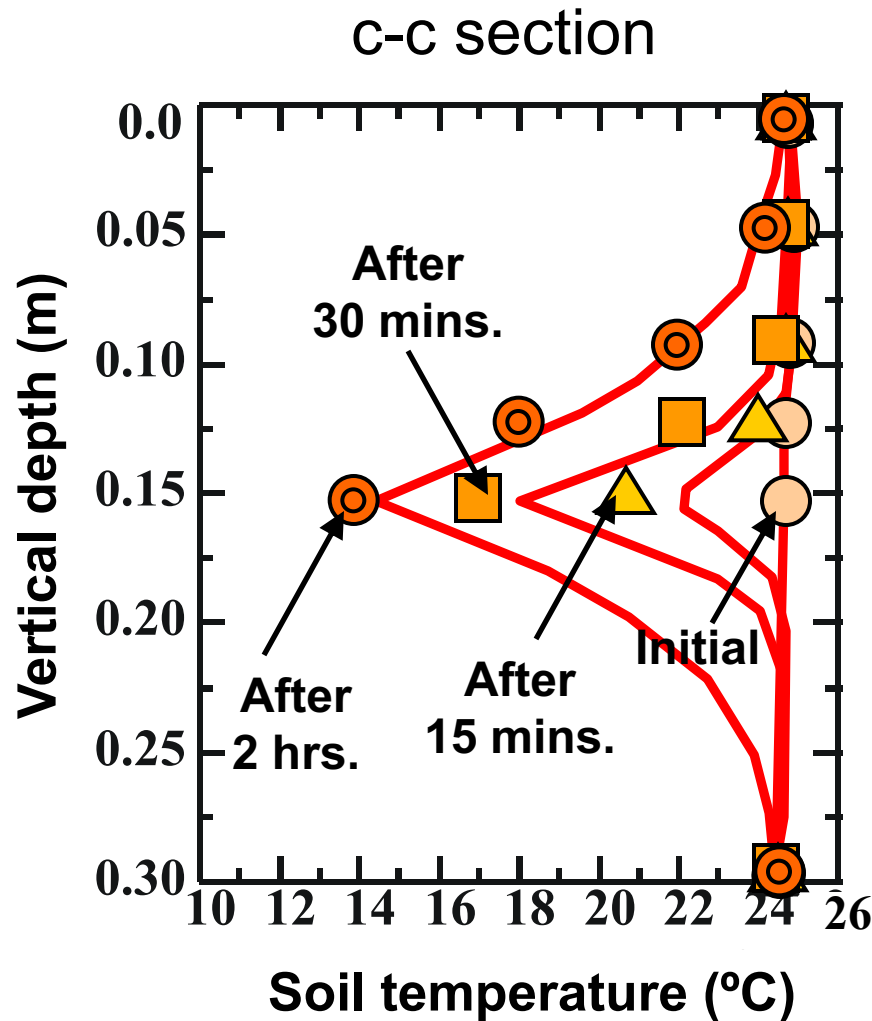


# Time change of HUT fluid temperature



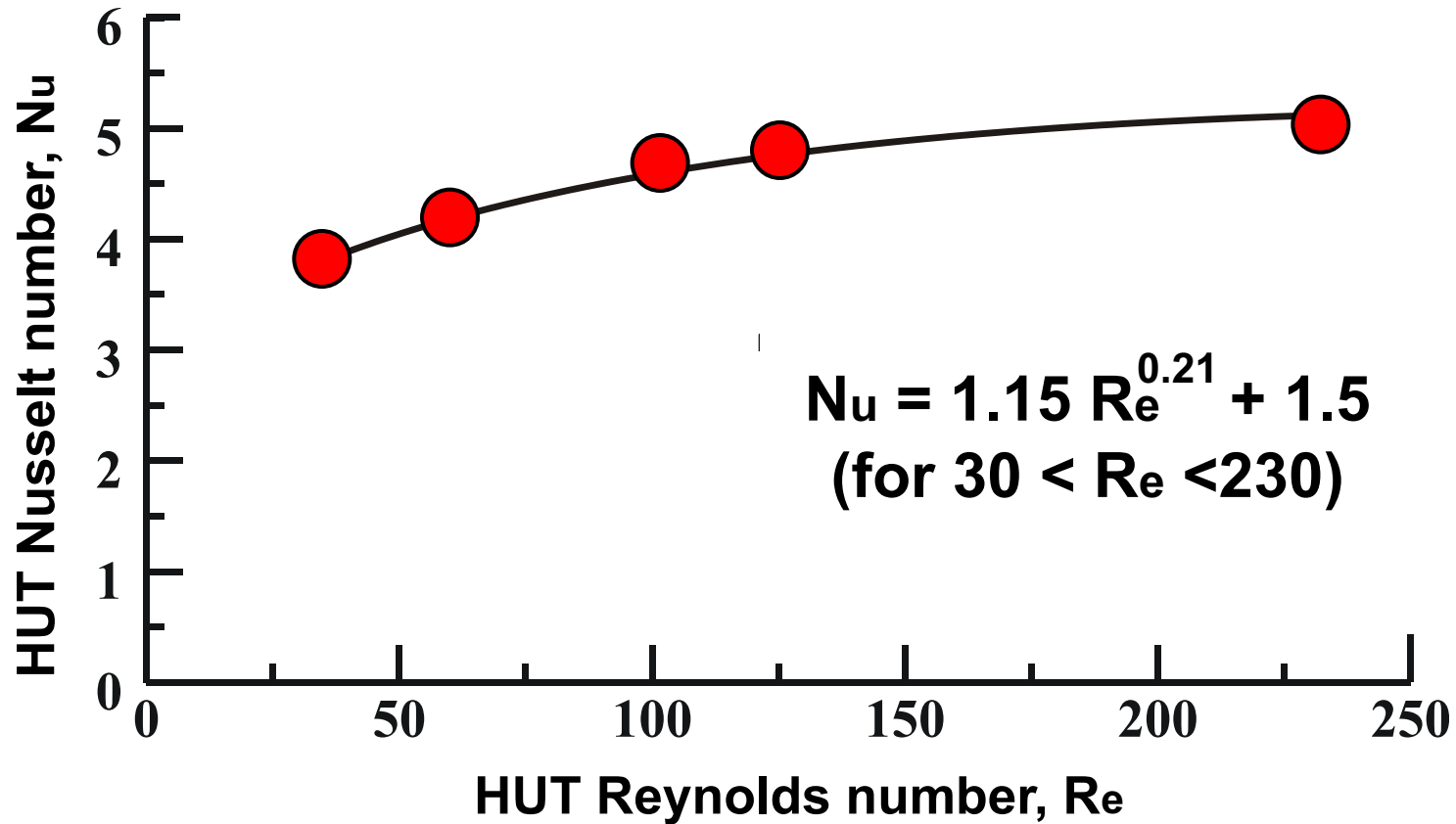
Flow rate:  $12.4 \times 10^{-7} \text{ m}^3/\text{sec}$

# Vertical ground temperature



$$\alpha = 46 \text{ W/m}^2\text{K}$$

# Relation between $Nu$ and $Re$



# Conclusions

A simplified heat transfer theory of a Horizontal U-Tube (HUT) is proposed and the applicability of the proposed model was discussed in comparison with experimental results using a miniature HUT

1. The relation between the HUT Nusselt number and the HUT Reynolds number is given by a power function and  $Nu$  increases with  $Re$ .
2. The indoor experimental results allowed the proposed model to reasonably predict the extracted ground heat.

**Thank You**

## 2.3 Initial & Boundary Conditions for Indoor Examination

### Initial Conditions

- Horizontal and vertical soil temperature
- Fluid temperature at the inlet of HUT

### Boundary Conditions

- Room temperature = 25 °C
- Relative Humidity = 50 %
- Time variations of the boundary soil temperatures were interpolated from the observed data obtained at an interval of 30 seconds.

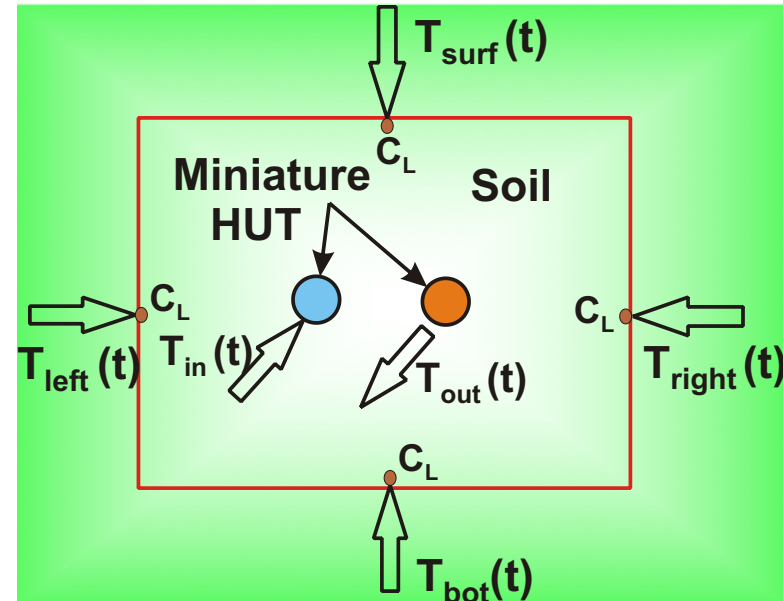


Fig. 9 Boundary conditions for indoor examination



## 3.2 Results of Indoor Experiments

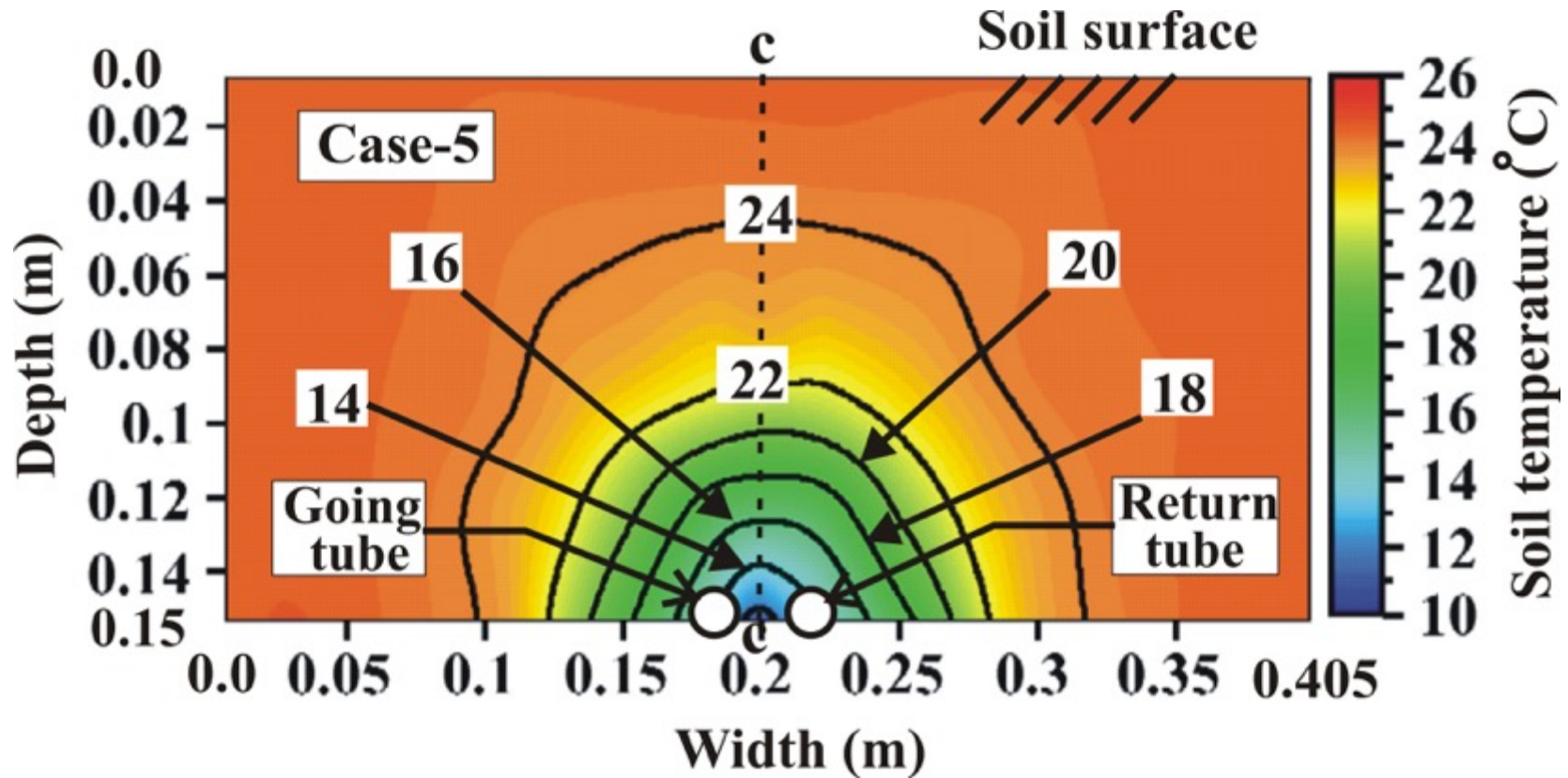
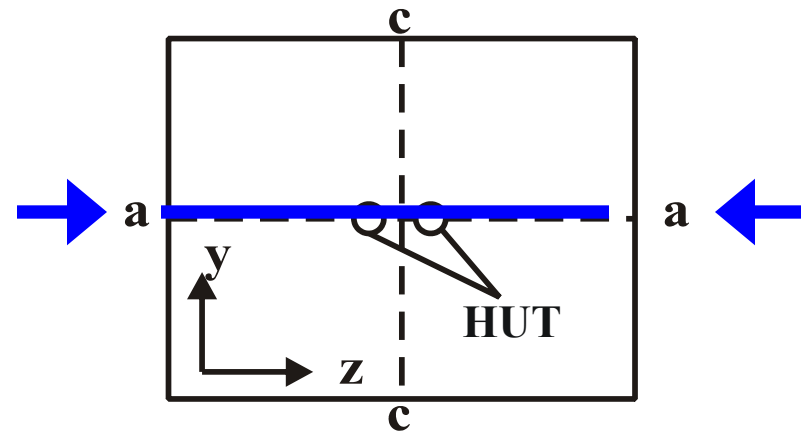
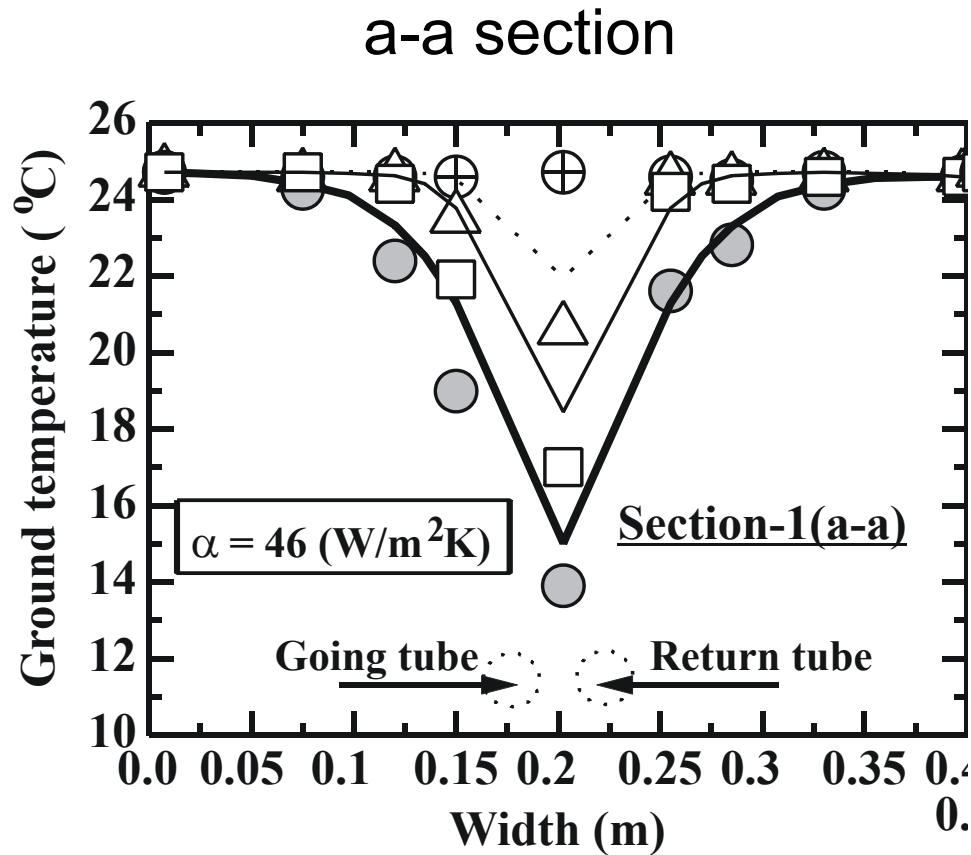
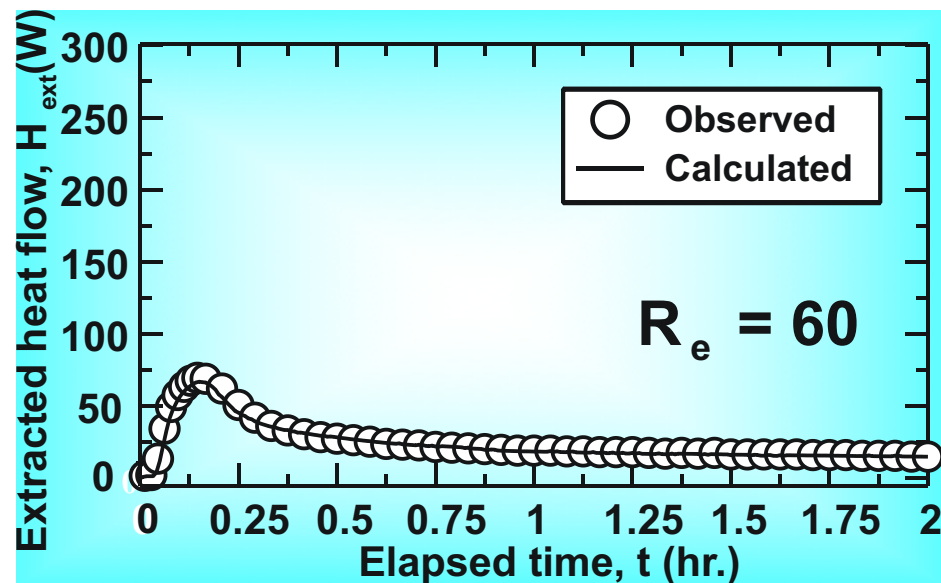


Fig. 18 Observed and calculated isothermal contours after 1.5 hours system operation (Case-5)

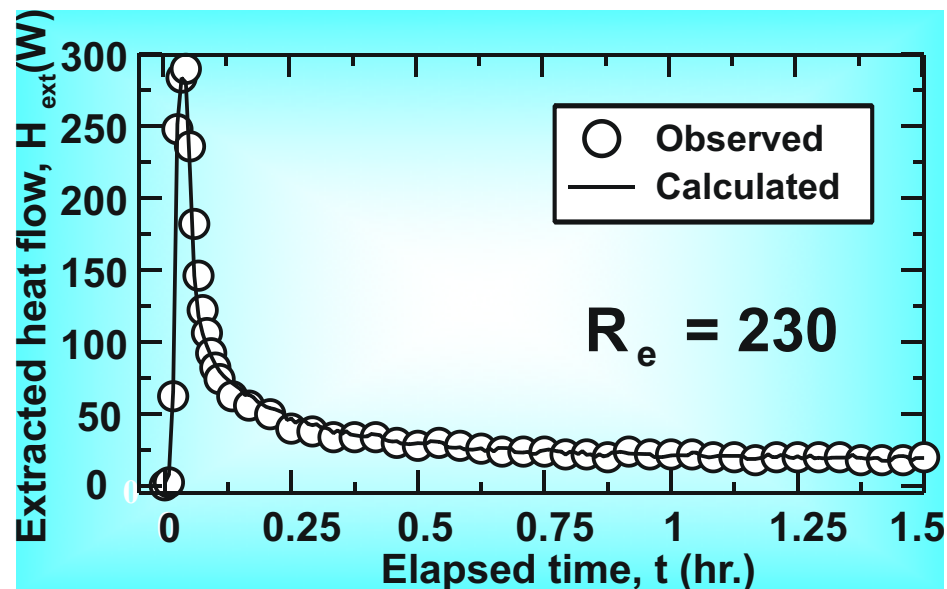
# Horizontal ground temperature



# 3.2 Results of Indoor Experiments



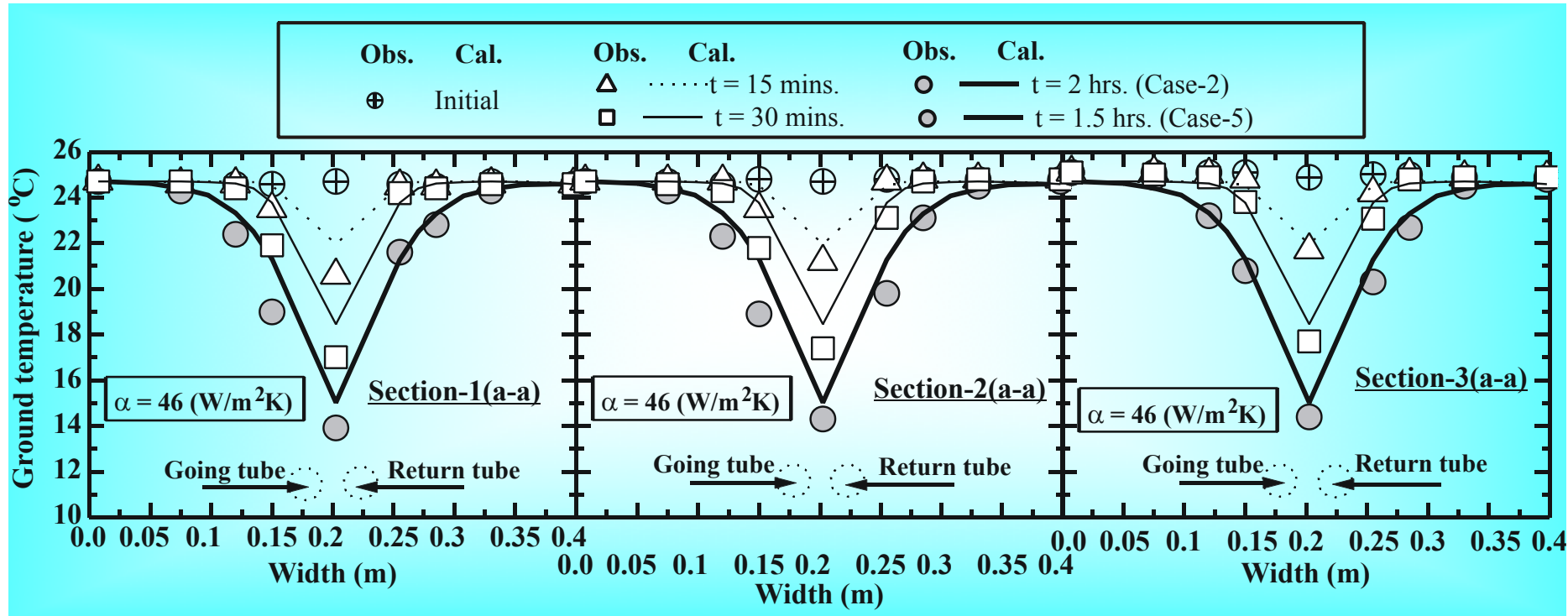
Case-2



Case-5

Fig. 20 Extracted heat flow with elapsed time

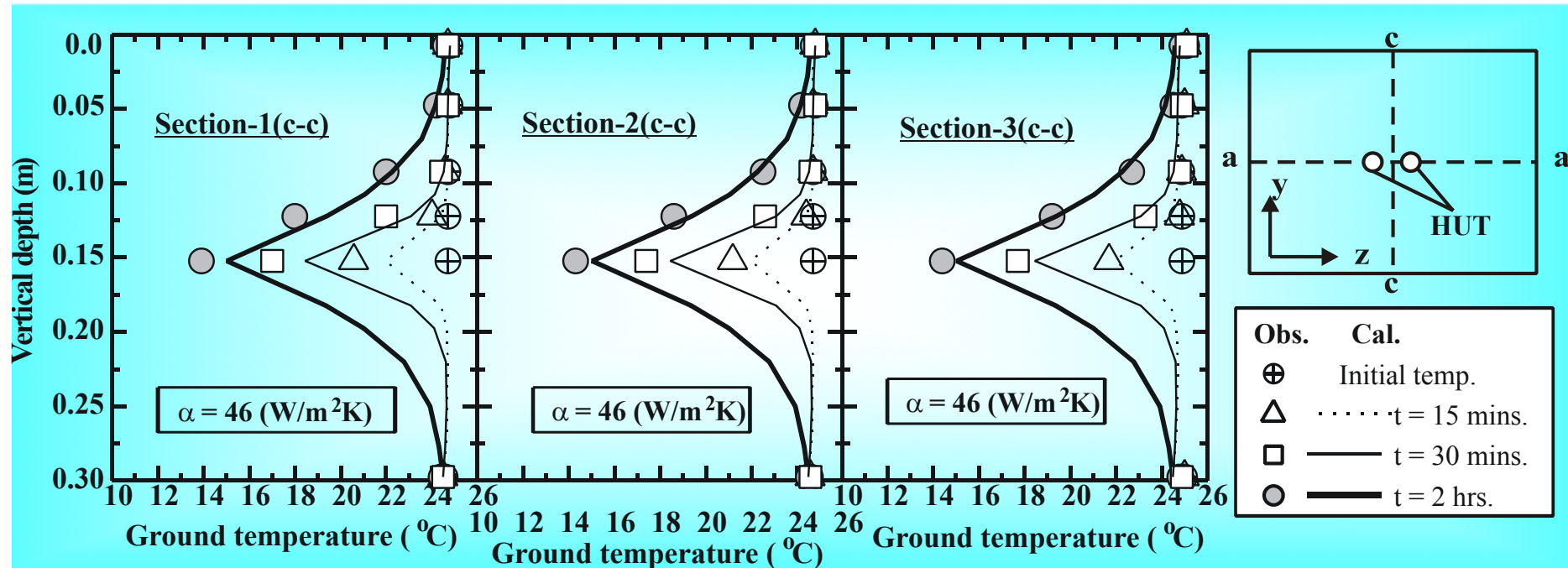
# 3.2 Results of Indoor Experiments



Case-2

Fig. 16 Model verification based on the horizontal ground temperature profile

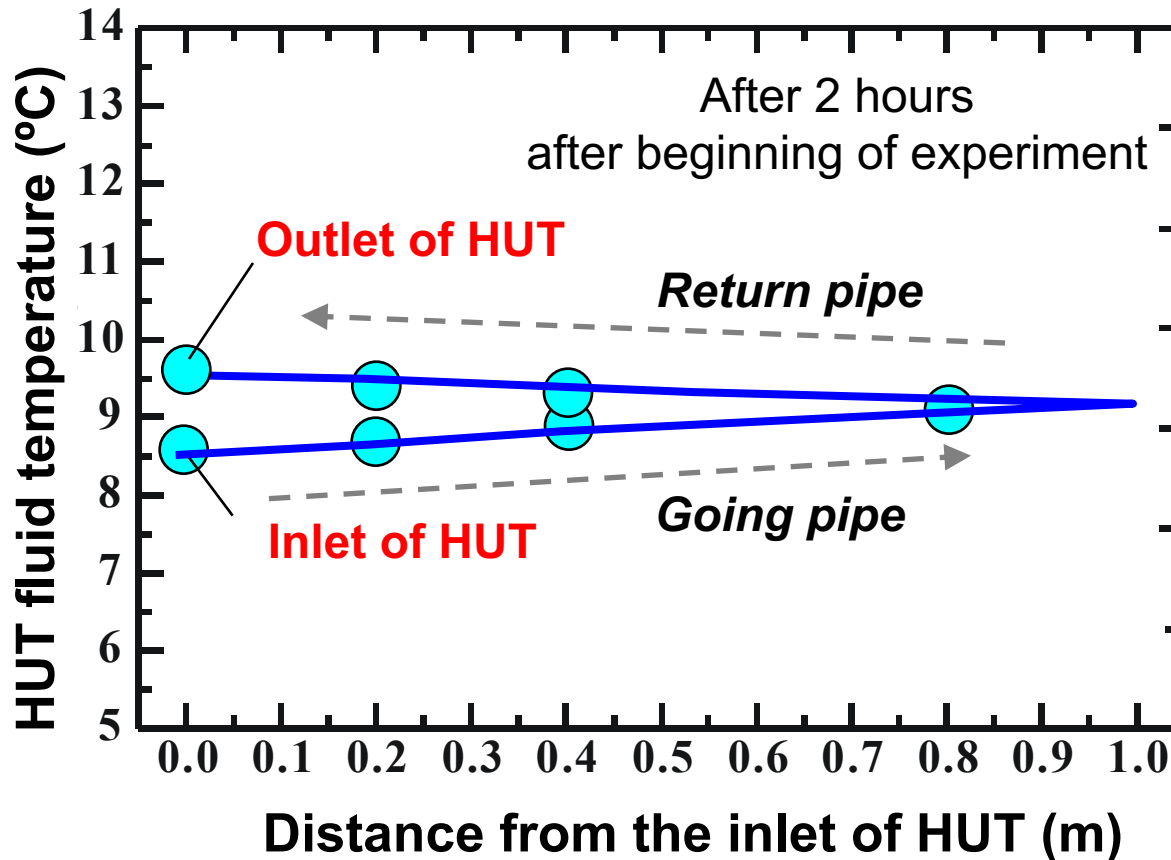
# 3.2 Results of Indoor Experiments



Case-2

Fig. 15 Model verification based on the vertical ground temperature profile

# Longitudinal profile of HUT fluid temperature



Flow rate:  $12.4 \times 10^{-7} \text{ m}^3/\text{sec}$